

## IMPROVED METHOD FOR THE PRODUCTION OF BACTERIAL TOXINS

### CROSS REFERENCE TO RELATED APPLICATIONS

**[0001]** This application claims priority to U. S. Provisional Application No. 60/194,478, filed April 4, 2000, which application is incorporated by reference in its entirety.

### REFERENCE TO SEQUENCE LISTING, TABLES OR COMPUTER PROGRAM LISTING

**[0002]** A Sequence Listing in computer readable format is included herewith.

### BACKGROUND OF THE INVENTION

**[0003]** The present invention relates to increasing bacterial toxin production using methods and compositions that reduce, or eliminate, the accumulation of intracellular and extracellular toxin expression inhibitors. Specifically, the present invention related to methods and compositions for reducing or elimination the accumulation of Bordetella species toxin expression inhibitors. More specifically, the present invention relates to the high yield production of pertussis toxin, pertactin, adenylate cyclase toxin-hemolysin, filamentous hemagglutinin and other toxins.

**[0004]** Pertussis toxin (PT) is one of the various components produced by virulent B. pertussis, the microorganism that causes whooping cough. Whooping cough is a serious infection of the respiratory system that at one time was responsible for the death of 5,000 to 10,000 people in the United States each year. Since the advent of the whooping cough vaccine the number of whooping cough related deaths has been reduced to less than 20 annually. Currently, about 50% of all whooping cough infections occur in children less than 1 year old, and only 15% occur in children over than 15 years old. Kids Health.org (visited March 23, 2000) <[http://kidshealth.org/parent/common/whooping\\_cough.html](http://kidshealth.org/parent/common/whooping_cough.html)>.

**[0005]** PT is a major protective antigen in the vaccine against whooping cough. Other components of interest produced by B. pertussis are filamentous hemagglutinin, heat labile

toxin, adenylate cyclase and the like, which may also play important role as protective antigens. Large-scale production of these components, which are useful as diagnostic or chemical reagents and in the preparation of vaccines, requires large-scale cultivation of the microorganism. However, *B. pertussis* is a fastidious organism that has proved difficult to grow in large fermentors. Older methods for the culture of *B. pertussis* employ cultivation in stationary culture or in fermentors. Growth in a stationary culture is labor intensive, while cultivation on a fermentation scale requires vortex stirring and surface aeration. As a result, the effective volume of the fermentor is reduced and modification of the fermentor for growth of pertussis is often necessary. Furthermore, the quantities of PT produced during fermentation under these conditions are variable and often low.

**[0006]** U.S. Patent No. 5,338,670 discloses a method for the production of *B. pertussis* in the presence of an iron salt, namely ferrous sulfate. While high iron content supports greater bacterial growth, it suppresses the production of PT. By adjusting the iron content of modified Stainer-Scholte media to 10% of the recommended concentration, the production of PT was optimized.

**[0007]** The present invention seeks to improve the yield of PT obtained from *B. Pertussis* by (1) introducing a soluble salt into the growth medium that sequesters sulfate ( $\text{SO}_4^{2-}$ ) and/or (2) employing a *B. pertussis* cysteine desulfinate knockout mutant.

#### BRIEF SUMMARY OF THE INVENTION

**[0008]** The present invention is based upon the discovery that bacterial toxin expression inhibitors accumulate in culture media and thus significantly reduce toxin production. Moreover, the present invention is based on the findings that suppressing or eliminating toxin expression inhibitors can significantly up regulate toxin expression. Non-limiting examples of the present invention are disclosed using *Bordetella* sp., specifically, *B. pertussis* and/or *B. bronchiseptica* which produce pertussis toxin (PT) and pertactin respectively. However, it is understood, that higher bacterial toxin levels can be achieved

in other bacterial culture systems using the teachings of the present invention including but not limited to adenylate cyclase toxin-hemolysin, and filamentous hemagglutinin.

**[0009]** Generally, the present invention is exemplified by disclosing methods and compositions used to cultivate *B. pertussis* that eliminate, or reduce, intracellular and extracellular PT inhibitor accumulation resulting in significant PT production increases.

**[0010]** In one embodiment of the present invention methods and compositions for preparing novel culture media that support *B. pertussis* growth and prevent or decrease PT inhibition expression by sulfate anions are disclosed. These media compositions and related methods include, but are not limited to, admixing a *B. pertussis* culture medium with an effective amount of one or more soluble metal salts that form substantially insoluble complexes with sulfate anions.

**[0011]** In another embodiment of the present invention culture media that support *B. pertussis* growth comprising an amount of one or more soluble salts that form substantially insoluble complexes with PT inhibitors, wherein said amount prevents or reduces the inhibition of PT expression are provided. Specifically, soluble metal salts are disclosed that form substantially insoluble complexes with sulfate anions.

**[0012]** Other embodiments of the present invention include *B. pertussis* culture media and methods for making and using same that reduce PT inhibitors by limiting or eliminating media constituents that contribute to PT inhibitor accumulation. Specifically, in one embodiment of the present invention cysteine concentration is reduced.

**[0013]** The invention also relates to methods and compositions for producing PT comprising cultivating *B. pertussis* under conditions that eliminate, or reduce, the accumulation of PT inhibitors in the culture media resulting in significant PT production increases and isolating the PT from the culture medium.

**[0014]** In yet another embodiment of the present invention PT production is enhanced using *B. pertussis* cysteine desulfase knockout mutants. In one embodiment of the present invention methods of producing PT comprising growing a *B. pertussis* cysteine

desulfinate knockout mutant in a *B. pertussis* culture medium, and isolating the PT from the culture medium are provided.

#### BRIEF DESCRIPTION OF THE DRAWINGS

**[0015]** FIG. 1: Graph showing the growth of *B. pertussis* (OD 650) as well as changes in the amounts of PT ([Ptx]/OD) produced as a function of fermentation time.

**[0016]** FIG. 2: Picture of a blood agar plate.

**[0017]** FIG. 3: Bar graph showing growth of *B. pertussis* (OD 650) and amount of PT (Ptx Conc.) in control culture supernatant (Ctr.), culture medium containing molecules <3,000 KDa (<3K) from spent culture media, and culture medium containing molecules >3,000 KDa (>3K) from spent culture media.

**[0018]** FIG. 4A: Graph of fermentation time (hours) vs. aspartic acid, threonine, cysteine and lysine concentration (mg/L) and arginine, methionine and proline concentration (mg/L) demonstrating the amino acid profiles during fermentation.

**[0001]** FIG. 4B: Graph of time (hours) vs. area (mAU $\times$ sec) demonstrating changes in the organic acid concentrations as a function of fermentation time.

**[0020]** FIG. 5: Bar graph showing sulfate concentration ( $\mu$ g/mL) at various culture times.

**[0021]** FIG. 6: Graph demonstrating the effect of increasing concentrations of BaCl<sub>2</sub> (mM) on the amount of PT produced ( $\mu$ g/ml/OD<sub>650</sub>) for two *B. pertussis* strains (strain 1= CS-87, strain 2= ATCC 9797).

**[0022]** FIG. 7: Depicts a comparison of the DNA sequence and translated amino acid sequence of the cysteine desulfinate gene isolated from *B. pertussis* strain BP536 with the *B. pertussis* sequence (contig 314) found in The Sanger Centre DNA data base.

**[0023]** FIG. 8a: Graphically depicts total B pertussis toxin production in 20 liter fermentors under limiting cysteine conditions measure at 600 nm absorbance.

**[0024]** FIG. 8b: Graphically depicts B pertussis toxin production in 20 liter fermentors under limiting cysteine conditions measured as mg/mL of toxin per optical density unit.

**[0025]** FIG. 9: Graphically depicts internal and external sulfate concentrations in B. pertussis cells in 20 liter fermentors in limiting cysteine conditions.

## DETAILED DESCRIPTION OF THE INVENTION

**[0026]** The most serious consequences of bacterial infections often result from toxin expression in the host. Non-limiting examples include, Clostridium tetani which produces tetanus toxin, neurotoxins produced by C. botulinum, C. difficile which produces toxins that cause pseudomembranous colitis, Salmonella typhi produces enterotoxins that cause gastroenteritis and typhoid fever, Staphylococcus aureus can express toxins that cause septic shock and B. pertussis produces toxins responsible for whooping cough. Other toxogenic genera of bacteria include, but are not limited to, Escherichia, Shigella, and Vibrio. Fortunately, vaccines are available that prevent and/or palliate the most severe effects of bacterial toxins. These vaccines are primarily composed of modified bacterial toxins, sub-lethal doses of purified toxin and or/or whole cell homogenates.

**[0027]** Bordetella pertussis vaccines have proven particularly effective in preventing whooping cough in vaccine recipients. Acellular pertussis (AP) vaccines containing Pertussis toxin (PT) alone or in combination with other antigens of B. pertussis have been found to be very effective in the prevention of pertussis infections. However, because PT and many of the other pertussis antigens are expressed in minute quantities, it is important to optimize culture conditions to maximize yields. Using the standard Stainer-Scholte (SS) media, a reduction in the pertussis toxin/optical density (PT/OD<sub>650</sub>) ratio midway through batch fermentations was observed. To determine whether this phenomenon was due to a lack of substrate availability or negative feedback inhibition, studies were conducted to determine whether spent media contained inhibitory factors for PT expression and to

identify these factors. Culture supernatant samples were taken from various stages of fermentation and re-supplied with SS media components lacking the basic salts. These samples were used to initiate a second culture and PT/OD<sub>650</sub> ratios measured as compared to fresh SS media. Both intact spent media and a fraction of this media containing molecules <3,000 kDa inhibited the production of PT. Cross-streaking experiments on Bordet-Gengou Agar (BGA) confirmed the production of inhibitor(s) of hemolytic activity in freshly streaked bacteria. Coomassie stained gels showed that the whole cell protein profiles were significantly different in the fraction media compared to fresh media suggesting that the inhibitory factors were influencing the two component regulatory system. To further identify these inhibitory compound(s), a complete flux analysis of the intermediate metabolism of *B. pertussis* was performed including amino acid and organic acid analysis by HPLC of the spent media as well as crucial enzymes within these pathways. The sulfur-containing amino acid, methionine, and pyruvate, were found to accumulate during late exponential phase of growth (up to 200 mg/L). Examination of all supernatant fractions by LC-MS suggests that pathways for cysteine consumption lead to the formation of sulfate. This in turn acted as a negative feedback inhibitor of PT expression.

**[0028]** Since sulfate acts as an inhibitor of PT expression in *B. pertussis*, methods were developed for reducing or eliminating intracellular and extracellular sulfate accumulation as the fermentation proceeds. In one embodiment of the present invention these methods include the addition of an effective amount of a soluble salt that forms a substantially insoluble complex with sulfate. Such soluble salts include alkali earth metal salts or other salts of Pb and Ag. Preferred salts of the present invention are alkali earth metal salts. More preferred salts are Ba(II) halide salts. The most preferred Ba(II) halide salt is BaCl<sub>2</sub> or BaBr<sub>2</sub>.

**[0029]** Barium chloride has been shown to be effective in promoting an increase in the amount of PT produced by *B. pertussis*. A ten-fold increase per OD unit in the yield of PT was observed when the ATCC 9797 or CS87 *B. pertussis* strain was cultivated in the presence of BaCl<sub>2</sub>. In this case, the amount of PT in the absence of BaCl<sub>2</sub> was 0.05

$\mu\text{g/mL/OD}_{650}$  as compared to  $0.525 \mu\text{g/mL/OD}_{650}$  with 20 mM  $\text{BaCl}_2$ . By "effective amount" of a salt is meant an amount that prevents or reduces inhibition of PT expression by sulfate during fermentation compared to when the fermentation is performed in the absence of the salt.

**[0030]** The solubility of the sulfate complex is defined by the solubility product ( $K_{\text{sp}}$ ). The sulfate complex is defined as "substantially insoluble" when the  $K_{\text{sp}}$  is approximately  $1 \times 10^{-5}$  or less at  $25^\circ \text{C}$ . Preferably, the  $K_{\text{sp}}$  is from about  $1 \times 10^{-7}$  to about  $1 \times 10^{-10}$  at  $25^\circ \text{C}$ . Most preferably the  $K_{\text{sp}}$  is from about  $1 \times 10^{-8}$  to about  $1 \times 10^{-10}$  at  $25^\circ \text{C}$ . Solubility products that fall within the aforementioned ranges for selected sulfate complexes are shown in Table 1.

Table 1:  $K_{\text{sp}}$  Values for Selected Sulfate Complexes

Complex	$K_{\text{sp}}$ (at $25^\circ \text{C}$ ) <sup>a</sup>
$\text{BaSO}_4$	$1.05 \times 10^{-10}$
$\text{PbSO}_4$	$1.82 \times 10^{-8}$
$\text{SrSO}_4$	$3.42 \times 10^{-7}$
$\text{AgSO}_4$	$1.19 \times 10^{-5}$

<sup>a</sup>CRC Handbook of Chemistry and Physics-65<sup>th</sup> Ed., Weast (ed.), p. B-220 (1984).

**[0031]** The sulfate complexes shown in Table 1 are meant to be examples and, as such, are not meant to narrow the scope of the present invention. In addition, it should be noted that the sulfate complex need not be completely insoluble in the growth medium. The sulfate complex must simply be sufficiently insoluble to prevent or reduce inhibition of PT expression by sulfate.

**[0032]** The salts of the present invention may be added to the medium before or after the cultivation of *B. pertussis* is initiated. Alternatively, the salt may be admixed with the other components of the medium prior to or after the addition of the water used in the preparation of the medium, but before the introduction of the *B. pertussis* cells.

**[0033]** An amount of the salt that may be used in the present invention to promote an increase in the amount of PT produced during fermentation may be from about 0.05 mM to about 50 mM, more preferably, from about 10 mM to about 30 mM, most preferably, about 20 mM. Normally from about 10 mM to about 20 mM of the salt is effective to prevent or reduce inhibition of PT expression by sulfate. One of ordinary skill in the art can determine the optimal amount of salt that effectively prevents or reduces inhibition of PT expression in any particular *B. pertussis* strain with no more than routine experimentation.

**[0034]** In another embodiment the present inventors have determined that regulating media concentrations of toxin inhibitor precursors can reduce both intracellular and extracellular toxin inhibitor concentrations. For example, and not intended as a limitation, the present inventors have determined that the PT inhibitors including, but not limited to, sulfites and sulfates are produced as end products of cysteine metabolism. Briefly, *Bordetella* metabolizes the sulfur containing amino acid cysteine via a pathway involving the enzyme cysteine desulfhinase. During cysteine metabolism, a sulfhydryl group is enzymatically cleaved from the cysteine molecule. This sulfhydryl group is further metabolized into sulfites and sulfates that accumulate within the bacterial cell and the extracellular milieu. Consequently, the longer *Bordetella* is grown in the presence of cysteine, the higher the intracellular and extracellular sulfate concentrations become and the less PT produced.

**[0035]** Based on the relationship between initial culture media cysteine concentrations and final sulfate concentrations, the present inventors developed the non-limiting theory that reducing the initial cysteine concentrations would result in reduced intracellular and extracellular sulfate accumulation and consequently, reduced PT inhibition. To evaluate the effect that varying cysteine concentrations have on sulfate concentration, the present inventors developed a three different culture systems identified using the following abbreviations: LCMSSB, LCMSSFB and LCMSSBa. The LCMSSB (limiting cysteine modified Stainer-Scholte batch) culture system consisted of *B. pertussis* grown in batch mode using the media as shown in Table 2 below. Briefly, "batch mode" is a process whereby micro-organisms are cultured in a single culture medium, usually liquid or semi-



liquid, without replenishing or exchanging a significant amount of the spent, or used, culture media. In the present invention batch mode cultures (LCMSSB) were incubated aerobically at between approximately 35°C and 37°C until bacterial optical densities reached >1.0 absorbance units as measured spectrophotometrically at 600 nm using procedures known to those skilled in the art. The second culture systems LCMSSFB (limiting cysteine modified Stainer-Scholte fed batch) was maintained using the culture media disclosed in Table 3. Note that no cysteine was added to the basal media. Instead, L-cysteine was added at a rate of 20 mg/hour for the entire incubation period. The final culture system was designated LCMSSBa (limiting cysteine modified Stainer-Scholte batch plus BaCl<sub>2</sub>) and used the basal media depicted in Table 2.

**[0036]** All three culture systems were inoculated and maintained as follows: Bordetella cultures were incubated at between approximately 35°C and 37°C in 20 liter bioreactors (New Brunswick BioFlo IV® (New Brunswick Scientific, Edison NJ) connected to an AFS Biocommand v2.0 (New Brunswick Scientific, Edison NJ) which collected data for pH, agitation, dissolved oxygen, temperature, and air flow rate. Additional pumps for anti-foam agents and pH control reagents were added as needed as known to those of ordinary skill in the art. Airflow was adjusted to 4.0 liters per minute, dissolved oxygen was maintained at 40% and pH was maintained at approximately 7.2.

**[0037]** Each 20-liter bioreactor contained 11 liters of test media and was inoculated with one liter of actively growing bacterial starter culture. The actively growing started cultures were prepared by inoculating shaker flasks containing one liter of Stainer Scholte (SS) medium, the formula of which is depicted in Tables 5 and 6, with frozen seed and incubated until an optical density of >1.0 OD<sub>600</sub> was reached (approximately 20–24 hours).

**[0038]** The inoculated fermentors were sampled at 3-6 hour intervals and separated into culture supernatants and cell pellets using centrifugation. The culture supernatants were assayed for PT, sulfates, organic acids, amino acids and bacterial density. Bacterial cell pellets were analyzed for internal sulfate and PT concentrations. Each culture system received a specific supplement(s) when culture bacterial population densities reached

approximately >1.0 absorbance units (approximately 12 hours post inoculation). Both LCMSSB and LCMSSBa received 200 mL of the amino acid supplement described in Table 4 below in addition to 10.0 mg/L  $\text{FeSO}_4 \bullet 7\text{H}_2\text{O}$  and 5.0 g/L monosodium glutamate (the  $\text{FeSO}_4$ /glutamate supplement). The LCMSSBa culture also received sufficient 1mM  $\text{BaCl}_2$  to obtain a final culture media concentration of 20 nM  $\text{BaCl}_2$ ; the LCMSSFB cultures received the  $\text{FeSO}_4$ /glutamate supplement with additional amino acids excluding cysteine and no  $\text{BaCl}_2$ . After supplementation, the fermentors were incubated as before until the experiments were terminated.

Table 2: Components of the LCMSSB Medium.

Component	Amount (g/L)
Sodium Chloride	2.5
$\text{KH}_2\text{PO}_4$	0.5
KCl	0.2
$\text{MgCl}_2 \bullet 6\text{H}_2\text{O}$	0.1
$\text{CaCl}_2$	0.02
TRIS Base	1.525
Ascorbic Acid	0.02
Glutathione	0.10
L-Cysteine Monohydrochloride	0.04
$\text{FeSO}_4 \bullet 7\text{H}_2\text{O}$	0.0010
Niacin	0.004
L-Arginine Monohydrochloride	0.40
L-Asparagine	0.10
L-Aspartic Acid	0.04
L-Histidine	0.03
L-Isoleucine	0.10

L-Leucine	0.10
L-Lysine Monohydrochloride	0.08
L-Methionine	0.03
L-Phenylalanine	0.03
L-Serine	0.06
L-Threonine	0.04
L-Tryptophan	0.01
L-Valine	0.04

Table 3: Components of the LCMSSFB Medium.

Component	Amount (g/L)
Sodium Chloride	2.5
KH <sub>2</sub> PO <sub>4</sub>	0.5
KCl	0.2
MgCl <sub>2</sub> •6H <sub>2</sub> O	0.1
CaCl <sub>2</sub>	0.02
TRIS Base	1.525
Ascorbic Acid	0.02
Glutathione	0.10
FeSO <sub>4</sub> •7H <sub>2</sub> O	0.0010
Niacin	0.004
L-Arginine Monohydrochloride	0.40
L-Asparagine	0.10
L-Aspartic Acid	0.04
L-Histidine	0.03

L-Isoleucine	0.10
L-Leucine	0.10
L-Lysine Monohydrochloride	0.08
L-Methionine	0.03
L-Phenylalanine	0.03
L-Serine	0.06
L-Threonine	0.04
L-Tryptophan	0.01
L-Valine	0.04

Table 4: Components of the Amino Acid Supplement

L-Cysteine Monohydrochloride	0.05
L-Arginine Monohydrochloride	0.40
L-Asparagine	0.10
L-Aspartic Acid	0.04
L-Histidine	0.03
L-Isoleucine	0.10
L-Leucine	0.10
L-Lysine Monohydrochloride	0.08
L-Methionine	0.03
L-Phenylalanine	0.03
L-Serine	0.06
L-Threonine	0.04
L-Tryptophan	0.01
L-Valine	0.04

**[0039]** All three reduced cysteine culture systems (LCMSSB, LCMSSFB and LCMSSBa) were tested in parallel with conventional SS media having cysteine concentrations as known in the prior art. Bordetella bacterial and PT concentrations are graphically depicted in FIGs. 8a and 8b. It can be seen from FIG. 8a that maximum Bordetella cell concentrations were reached at approximately 32 hours. Maximum growth was nearly identical when normal PT production media is compared with modified SS in batch mode. FIG. 8b depicts maximum PT production as measure in mg/ml of culture media. It is readily apparent that a significant improvement in overall PT production is realized using any of the cysteine limiting culture systems of the present invention when compared to conventional culture systems. Moreover, FIG. 9 depicts internal and external sulfate concentrations in *B. pertussis* cells in 20 liter fermentors in limiting cysteine conditions. The LCMSSBa culture system demonstrated the best improvement in overall PT production. Therefore, as theorized by the present inventors, PT production can be significantly improved by limiting the amount of inhibitor precursor in the culture media. Moreover, even further improvement can be realized when the precursor limiting culture systems of the present invention are combined with the toxin expression inhibitor removal systems of the present invention.

**[0040]** The present inventors have demonstrated that: 1) specific toxin expression inhibitors that accumulate in the media of toxin producing bacteria can significantly reduce overall toxin production; and 2) that removal of toxin expression inhibitors from the culture media, or reduction in toxin inhibitor formation by reducing inhibitor precursors in the culture media, can significantly increase overall toxin production. Therefore, the present inventors theorized that genetically disabling a toxin producing organism's ability to produce a toxin expression inhibitor might yield similar increases in overall toxin production. Consequently, in yet another embodiment of the present invention a recombinant *B. pertussis* lacking cysteine desulfonase activity ("knockout mutant") that does not produce sulfate in culture and, thus, does not exhibit inhibited PT expression is provided. Such knockout mutants may be prepared by anyone of a number of different methods. See, for example, U.S. Pat. Nos. 5,557,032 and 5,614,396. Such methods, in general, involve homologous recombination of a DNA construct with *B. pertussis* chromosomal DNA. Homologous

recombination is a well-studied, natural cellular process which results in the scission of two nucleic acid molecules having identical or substantially similar sequences (i.e. homologous), and the ligation of the two molecules such that one region of each initially present molecule is ligated to a region of the other molecule. (See Sedivy, J.M., BioTechnol. 6:1192-1196 (1988)). Homologous recombination is, thus, a sequence specific process by which cells can transfer a "region" of DNA from one DNA molecule to another. For homologous recombination to occur between two DNA molecules, the molecules must possess a "region of homology" with respect to one another. Such a region of homology must be at least two base pairs long. Two DNA molecules possess a region of homology when one contains a region whose sequence is so similar to a region in the second molecule that homologous recombination can occur. Where a particular region is flanked by two regions of homology, then two recombination events may occur, resulting in an exchange of regions between the two recombining molecules. Homologous recombination is catalyzed by enzymes that are naturally present in *B. pertussis*.

**[0041]** In one such method, the gene coding for cysteine desulfinate (Figure 7), e.g. contained within a plasmid, is cut with restriction enzymes selected to cut within the gene such that a new DNA sequence encoding a marker gene can be inserted within the cysteine desulfinate gene sequence. This marker gene will serve to prevent expression of the cysteine desulfinate gene. The marker gene can be any nucleic acid sequence that is detectable and/or assayable, however, in a preferred embodiment, it is an antibiotic resistance gene. The marker gene may be operably linked to its own promoter or to another strong promoter from any source that will be active or easily activatable in *B. pertussis*. In another embodiment, the marker gene may be transcribed using the promoter of the cysteine desulfinate gene. The marker gene may have a poly A sequence attached to the 3'-end of the gene to terminate transcription. Preferred marker genes include any antibiotic resistance gene such as *ermC'* (the erythromycin resistance gene), *neo* (the neomycin resistance gene), *amp* (the ampicillin resistance gene), *kan* (the kanamycin resistance gene) and *gent* (the gentamicin resistance gene).

**[0042]** After the DNA sequence has been digested with the appropriate restriction enzymes, e.g. SphI and SphI or PstI and PstI, the marker gene sequence is ligated into the cysteine desulfinate DNA sequence using methods well known to the skilled artisan and disclosed, for example, in Sambrook et al. (Molecular Cloning: A Laboratory Manual, Cold Spring Harbor Laboratory Press, Cold Spring Harbor, N.Y. (1989)). The ends of the DNA fragments to be ligated must be compatible; this is achieved by either cutting all fragments with enzymes that generate compatible ends, or by blunting the ends prior to ligation. Blunting is done using methods well known in the art, such as for example, by use of Klenow fragment (DNA polymerase I) or other DNA polymerase to fill in sticky ends. This construct contains DNA sequences corresponding to defined regions of the cysteine desulfinate gene, e.g. corresponding to the 3'- and 5'-ends of the cysteine desulfinate gene, allowing for integration of the construct by homologous recombination. This DNA construct may be ligated into a plasmid having a second antibiotic resistance gene.

**[0043]** The construct may then be transfected into *B. pertussis* using known methods, e.g. by electroporation or by mating with transfected *E. coli* cells. Screening of the cells is accomplished by culturing the cells in the presence of otherwise lethal concentrations of one or more antibiotics corresponding to the antibiotic resistance genes that are present. Those cells that survive will have the knockout construct integrated therein. One may use a non-replicating plasmid so that the selected cells would not just have the plasmid construct therein. In order to confirm the integration of the knockout construct, a Southern Blot of the *B. pertussis* DNA can be probed with a sequence designed to hybridize only to the marker sequence and/or the portion of the cysteine desulfinate that is removed. Alternatively or additionally, the DNA can be amplified by PCR with probes corresponding to the 3'- and 5'-ends of the cysteine desulfinate gene. Finally, cysteine desulfinate activity may be assayed.

**[0044]** In another embodiment, *B. pertussis* may be cultivated in the presence of nucleotide sequences that are anti-sense to the coding sequence of the cysteine desulfinate gene. In this embodiment, the nucleotide sequences are taken up by *B. pertussis*, hybridize to the cysteine desulfinate-encoding gene, and inhibit translation of the

gene. Modified nucleotide sequences can also be employed which interact with the bases of the gene to form covalent bonds and thereby inhibit translation. See U.S. Pat. 6,015,676.

**[0045]** Examples of nucleotides which are antisense to the cysteine desulfase gene include any nucleotide of at least 8 bases, preferably, 10 to 15 bases, which are complementary to the coding region of Figure 7. Examples include:

GATTGCTGAT (SEQ. ID. NO. 1)

TAGATGGGGC (SEQ. ID. NO. 2)

**[0046]** In the present invention, a variety of media may be used to cultivate *B. pertussis*. Non-limiting, exemplary media include the Stainer Scholte and the GMAR modified media. The components of the Stainer Scholte and GMAR modified media are presented in Tables 2 and 3, respectively.

Table 5: Components of the Stainer Scholte Medium.<sup>b</sup>

Component	Amount (g/L)
L-Glutamic Acid Monosodium Salt	10.72
L-Proline	0.24
Sodium Chloride	2.5
KH <sub>2</sub> PO <sub>4</sub>	0.5
KCl	0.2
MgCl <sub>2</sub> •6H <sub>2</sub> O	0.1
CaCl <sub>2</sub>	0.02
TRIS Base	1.525
Ascorbic Acid	0.02
Glutathione	0.10



L-Cysteine	0.04
Nicotinic Acid	0.004
FeSO <sub>4</sub> •7H <sub>2</sub> O	0.010

<sup>b</sup> From: Hewlett and Wolff, J. Bacteriol. 127:890-898 (1976).

Table 6: Components of the GMAR Modified Medium.

Component	Amount (g/L)
L-Glutamic Acid Monosodium Salt	10.7
L-Proline	0.24
Sodium Chloride	2.50
KH <sub>2</sub> PO <sub>4</sub>	0.50
KCl	0.20
MgCl <sub>2</sub> •6H <sub>2</sub> O	0.10
CaCl <sub>2</sub> •2H <sub>2</sub> O	0.02
TRIS Base	1.52
Ascorbic Acid	0.02
Glutathione, Reduced	0.10
L-Cysteine	0.04
Niacin	0.004
FeSO <sub>4</sub> •7H <sub>2</sub> O	0.001
L-Arginine Monohydrochloride	0.40
L-Asparagine	0.10
L-Aspartic Acid	0.04
L-Cysteine Monohydrochloride	0.10
L-Histidine	0.03

L-Isoleucine	0.10
L-Leucine	0.10
L-Lysine Monohydrochloride	0.08
L-Methionine	0.03
L-Phenylalanine	0.03
L-Serine	0.06
L-Threonine	0.04
L-Tryptophan	0.01
L-Valine	0.04

**[0047]** The PT toxin produced by the methods of the current invention may be purified according to the method described by Sekura et al., J. Biol. Chem. 258:14647-14651 (1983). Briefly, the method of Sekura utilizes two consecutive chromatographic steps to purify PT. The first step involves chromatography on an Affi-gel blue column. The second step involves chromatography on a fetuin-agarose column. The PT purification method of Sekura et al. allows for the routine and rapid purification of PT in relatively large quantities (in excess of 10 mg). Alternatively, PT may be purified using a peptide affinity column. Such a column is described below in Example 1. In this embodiment, the PT is adsorbed onto the column, washed with buffer (e.g. 50 mM TRIS HCl, pH = 6.2), and the PT is then eluted with 4 M MgCl<sub>2</sub>. The MgCl<sub>2</sub> is removed by dialysis to give substantially pure PT.

**[0048]** Having now generally described this invention, the same will be understood by reference to the following examples which are provided herein for purposes of illustration only and are not intended to be limiting unless otherwise specified.

#### Example 1

##### Materials and Methods

**[0049]** Organisms: Wild-type B. pertussis strain CS87 was used for most of these studies. This strain originated in China and was brought to the National Institute of Child

Health and Human Development (NICHD) at the National Institutes of Health (NIH). In addition, several strains of BP were procured from the American Type Culture Collection (Manassas, VA), including, but not limited to ATCC number 10380 both of which are suitable for preparing the cysteine desulfinate knockout mutants disclosed herein. Organisms were stored at -70°C or maintained on BGA (BBL, Inc. Rockville, MD) in a humid incubator maintained at 37°C.

**[0050]** The medium utilized to culture the cells was similar to the defined medium described by Stainer and Scholte. J. Gen. Microbiol. 63:211-220 (1970). One liter of the medium contained: 10.7 g monosodium glutamate, 0.24 g proline, 2.5 g NaCl, 0.5 g  $\text{KH}_2\text{PO}_4$ , 0.2 g KCl, 0.1 g  $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$ , 20 mg  $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$ , 1.52 g Tris, 20 mg ascorbic acid, 100 mg glutathione, 40 mg cysteine, and 4 mg niacin. The salts, glutamate, and proline were prepared as a basal formulation and were autoclaved for sterilization. The rest of the medium (supplement) was prepared in concentrated form (100-fold) and filter sterilized. The final pH of the medium was between 7.2 and 7.5. In some experiments, 10 mg/L  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  was added. Organisms were grown either in triple baffled Erlenmeyer flasks in a New Brunswick Innova Model 4300 shaking incubator (New Brunswick Scientific, Edison, NJ) maintained at 37°C or in a New Brunswick 20 L BioFlo IV (New Brunswick Scientific) running in batch mode with a working volume of 12 L. The reactor was connected to an AFS Bio Command v.2.0 (New Brunswick Scientific), which collected data for pH, agitation, dissolved oxygen, temperature, air flow rate and additional pumps for antifoam and pH maintenance. The air flow rate in the fermentor was set at 0.125 vvm and the temperature was controlled at 36.5°C in all experiments. The dissolved oxygen (DO) was maintained at 40% by using an agitation cascade from 150 to 1000 RPM. The pH was controlled at 7.2 by the addition of 50%  $\text{H}_3\text{PO}_4$ .

**[0051]** The reactor was batched with approximately 11 L of defined medium and inoculated with an actively growing seed (1 L), for a total working volume of 12 L. Samples were drawn from the reesterilization sample port every 3 to 6 hours. For analysis of extracellular metabolites, the supernatant was filtered through a 0.2  $\mu\text{m}$  Millex-GV filter (Millipore Co., Bedford, MA) and stored at -20°C.

**[0052]** Growth of the culture was measured by optical density at 650 nm ( $OD_{650}$ ) using a Shimadzu UV Spec 120 (Shimadzu, Columbia, MD). Culture purity was verified by gram staining and plating on BGA (BBL, Inc. Rockville, MD) and trypticase soy agar (TSA; BBL, Inc.). A pure culture of *B. pertussis* would demonstrate all organisms staining gram-negative, growth on BGA agar and lack of growth on TSA agar.

**[0053]** Amino acid analysis: The analysis and quantification of amino acids were made by reverse phase high-pressure liquid chromatography (RP-HPLC) using an on-line pre-column derivatization, as provided for the AminoQuant column (Hewlett-Packard Co., Wilmington, DE). Primary acids were derivatized by the OPA reagent (10 mg/ml o-phthalaldehyde, 10 mg/ml 3-mercaptopropionic acid in 0.4 M borate buffer), while secondary amino acids were derivatized by FMOc reagent (2.5 mg/ml 9-fluorenylmethylchloroformate in acetonitrile). For primary amino acids, the mobile phase consisted of sodium acetate/tri-ethanolamine/tetrahydrofuran (pH  $7.2 \pm 0.05$ ) and were detected at 338 nm. Secondary amino acids were eluted using a sodium acetate/methanol/acetonitrile mobile phase (pH  $7.2 \pm 0.05$ ) and were detected at 262 nm. The identification of each amino acid was performed with a set of amino acid standards (Hewlett-Packard) at different concentrations (100, 250, and 1000 pmol/ $\mu$ l). HPLC Model HP-1050 (Hewlett-Packard) was utilized for these analyses in conjunction with the HP ChemStation software (Hewlett-Packard, v.2.0).

**[0054]** Organic Acid detection and quantification: Organic acids were detected using a Model HP-1050 HPLC (Hewlett-Packard) in conjunction with the HP ChemStation v.2.0 software and equipped with a BioRad Aminex HPX-87H column (Bio-Rad Laboratories, Burlingame, CA) having a mobile gas phase of 4 mM  $H_2SO_4$ . The column was equilibrated at 35°C and the isocratic flow rate was 0.6 ml/min. The detection was performed at 215 nm. The identification of each organic acid was achieved by injecting the Bio-Rad Organic Acid Analysis Standard (Bio-Rad Laboratories), which consisted of a mixture of sodium oxalate, sodium citrate, sodium maleate, sodium succinate, sodium formate, and sodium acetate. Pyruvate was assessed by spiking the organic acid standard with 2.5 g/l pyruvate.

**[0055]** Each of the organic acids were quantified using enzymatic kits and following the manufacturer's recommended protocol as follows: Citric acid, Boehringer-Mannheim kit 139-076 (Boehringer-Mannheim, Indianapolis, IN); succinic acid, Boehringer-Mannheim kit 176-281 (Boehringer-Mannheim, Indianapolis, IN); formic acid, Boehringer-Mannheim kit 979-732 (Boehringer-Mannheim, Indianapolis, IN); acetic acid, Boehringer-Mannheim kit 148-261 (Boehringer-Mannheim, Indianapolis, IN); oxalic acid, Boehringer-Mannheim kit 755-699 (Boehringer-Mannheim, Indianapolis, IN); and pyruvate, Sigma kit 726-UV (Sigma Chemicals Co, St. Louis, MO).

**[0056]** Quantitative PT ELISA Assay: Microtiter plates (Nunc-Immuno Plate IIF, Vangard International, Neptune, NJ) were sensitized by adding 0.1 ml per well of fetuin (Sigma Chemical Co.) at 0.2  $\mu$ g/ml in 0.1 M sodium carbonate, pH 9.6, and incubating overnight at room temperature. The plates were washed five times with a solution containing 0.9% NaCl, 0.05% Brij 35, 10 mM sodium acetate at pH 7.0, and 0.02% azide. Samples containing PT were diluted in PBS with 0.5% Brij 35 and added to the plate and incubated for 2 hr at room temperature. The plates were again washed as before and the monoclonal antibody to PT (20.6) was diluted with PBS. Ibsen, et al., Infect. Immun. 61:2408-2418 (1993). The plates were again washed and the secondary antibody, alkaline phosphatase conjugated goat anti-mouse IgG and IgM (Tago Inc., Burlingame, CA), was diluted in PBS-Brij, was added to the plates and was then incubated for 2 h at room temperature. The plates were washed as before and p-nitrophenyl phosphate (Sigma Phosphatase Substrate 104) (1 mg/ml), in a solution of 0.1 M diethanolamine, 1 mM  $MgCl_2$ , 0.1 mM  $ZnCl_2$ , and 0.02% azide, at pH 9.8, was added. The plates were incubated at 37°C for 1 h and the absorbance at 405 nm was determined using a Dynex Model MRX microtiter plate reader (Dynex Technologies, Inc., Chantilly, VA). For each plate, a standard curve was generated using purified PT (North American Vaccine, Inc.) diluted in 0.1% BSA and 0.1% glycerol in PBS. The concentration of PT from culture samples was calculated from the standard curve.

**[0057]** Sulfate Determinations: Sulfate concentrations within the medium were determined using the methods of Melnicoff, et al. The assay was adapted to a microplate assay. Melnicoff, et al., Res. Commun. Chem. Pathol. Pharmacol. 14:377-386 (1976).

**[0058]** Cloning of the *B. pertussis* *nifS*-like gene: The DNA fragment containing the *nifS*-like gene was amplified by a Perkin-Elmer Thermal Cycler 480. The reaction mixture (50  $\mu$ l) contained: 20 ng purified *B. pertussis* chromosomal DNA, 0.2  $\mu$ M of each primer (forward primer: 5' ATG AGC AAT CGC CCC ATC TAC 3' (SEQ. ID. NO. 3); reversed primer: 5' CAC TAT TTG GTC GGT CGG 3' (SEQ. ID. NO.4), 2 mM  $MgCl_2$ , 10 mM Tris-HCl (pH 8.3), 50 mM KCl, 400  $\mu$ M each dNTP, and 2.5 units of AmpliTaq Gold (Perkin Elmer, Branchburg, NJ). The conditions were as follows: first cycle, 2 min at 94°C; subsequent 35 cycles, 94°C (2 min), 42°C (1 min), 72°C (2 min); and with a final 72°C incubation time for 8 min. The PCR product was gel purified in a 1% agarose gel and ligated into pCR<sup>®</sup>II-TOPO (Invitrogen, Carlsbad, CA) using the conditions recommended by the manufacturer making pBPfilS. The plasmid pBPfilS was transformed into *E. coli* strain TOPF' (Invitrogen) and transformants were selected on LB-amp agar media. Sequencing was performed using an Applied Biosystems PRISM Model 310 Automated sequencer (Applied Biosystems, Inc., Foster City, CA) using the manufacturer's recommendations and sequencing kit.

**[0059]** Construction of a *B. pertussis* strain containing a null mutation in the BP filS-like gene: The pBPfilS plasmid made in accordance with the teachings of the present invention was cut with SphI and SphI as well as blunting the ends with the Klenow fragment of DNA polymerase (Boehringer Mannheim). The cut plasmid was gel purified and a blunt-ended erythromycin resistant gene (*ermC'*) or luciferase was ligated into the plasmid construction. Klugman, et al. Infect. Immun. 57:2066-2071 (1989). Transformants of DH5 were identified having resistance to 100  $\mu$ g of erythromycin per ml. The constructed plasmid was reisolated using Qiagen columns (Qiagen, Inc., Valencia, CA) and the mutated insert was isolated by cutting the plasmid with BamHI and XhoI. The insert was gel purified and ligated into the BamHI and XhoI site of plasmid pSS1129 to make pBP $\Delta$ filS. Stibitz, J. Bacteriol. 180:2484-2492 (1998). This was transformed into *E. coli* strain SM10 and the

transformants used to mate with *B. pertussis* strain BP536 as described by Stibitz. "Use of Conditionally Counterselectable Suicide Vectors for Allelic Exchange," in *Bacterial Pathogenesis*, Clark and Bavoil (eds.), p.301-308 (1997). *B. pertussis* isolates containing the null *BpfilS* gene within the chromosome were selected for gentamicin, streptomycin and/or erythromycin resistance or luciferase activity on BGA agar.

**[0060]** Miscellaneous: All materials were purchased from Sigma Chemical Co. and/or of the highest grade available. Total protein was quantified by Coomassie Protein Assay<sup>®</sup> (Pierce Chemical Co., Rockford, IL). Human IgG was used as the standard. *Bordetella pertussis* strain BP536, a spontaneous streptomycin resistant mutant of strain BP338, used in the transformation experiments was obtained from Dr. Scott Stibitz at the Center for Biological Research and Evaluation, United States Food and Drug Administration (Stibitz, S. and M-S. Yang. 1991. *J. Bact.* 173:4288-4296). The transformed *B. pertussis* knockout mutant derived therefrom was designated strain BP536pWY and has been deposited with the American Type Culture Collection, (Manassas, VA) in accordance with the terms of the Budapest Treaty. The American Type Culture Collection has assigned *B. pertussis* strain BP536pWY ATCC number \_\_\_\_\_. All methods employed are all well known to those of ordinary skill in the art. See for example: *Methods in Molecular Biology*, vol XX, B.D. Shepard and M.S. Gilmore (eds) (1995); *DNA Sequencing*, L. Alpey. Bios Scientific Publishers (1997); *Diagnostic and Molecular Microbiology: Principles and Applications*, D.H. Persing, T.F. Smith, F.C. Tenover and T.J. White (eds) (1993) American Society for Microbiology; *Molecular Biology*, D. Freifelder (ed) (1987) Jones and Bartlett Publishers; and *Molecular Biology of the Gene*, J.D. Watson, N.H. Hopkins, J.W. Roberts, J.A. Steiz and A.M. Weiner (eds) (1987) The Bengerman/Cummings Publishing Company, Inc.

## Results

**[0061]** Detection of Inhibitor(s) of PT production in broth cultures of BP: Samples were taken at various times during the growth phase of the BP cultures. The samples were monitored for BP growth by measuring the OD<sub>650</sub> and for the production of PT by ELISA. The results were calculated as PT in microgram/per ml/OD<sub>650</sub> in order to approximate the amount of PT produced per cell. As shown in Figure 1, the amount of PT produced per cell

fell drastically midway through the growth cycle. Although *B. pertussis* continued in logarithmic phase growth, the production of PT appeared to decrease almost to the total elimination of PT production. This suggested that an inhibitor of PT production was being generated during the early phases of the culture and that after reaching inhibitory concentration, PT production ceased. To test this hypothesis, culture supernatant from a *B. pertussis* culture grown to stationary phase was lyophilized and was reconstituted with growth media lacking the basic salts. This mixture was then used to grow a second culture of *B. pertussis* and was compared to the original media used for *B. pertussis*. Samples were taken and assayed as before. The growth of *B. pertussis* in each of the two media was similar with the OD<sub>650</sub> reaching approximately the same levels. However, the total amount of PT produced in the reconstituted mixture was drastically reduced compared to that in the original media. A more visual demonstration of such an inhibition, and that this inhibitor also effects the production of adenylate cyclase, the cause of haemolysis on blood agar plate, is shown in Figure 2. An initial streak of *B. pertussis* was made on a BGA plate and allowed to grow for 48 hrs. Secondary cross-streaks were then made and the agar plate was incubated for an additional 48 hrs. It can be seen that a zone of non-haemolysis radiates out from the initial growth streak. Characterization of the inhibitor began by filtering the spent culture media through a 3,000 MWCO filter retaining both the permeate and the filtrate. Both were lyophilized and reconstituted as before. Figure 3 demonstrates the results of the *B. pertussis* grown in these mixtures as compared to the GMAR media. The production of PT was inhibited by the permeate mixture suggesting that the inhibitor had a molecular weigh smaller than 3,000.

**[0062]** Amino Acid and Organic Acid Analysis: Both amino acid and organic acid analysis were performed on samples taken at different times during the course of a typical *B. pertussis* culture in order to determine whether the rise and/or the timing of the increase in these compounds correlated with the timing of the production inhibition of PT. These data are shown in Figures 4a and 4b. It should be noted that the drop in PT production occurs at approximately half way through the growth phase, typically at 20 h. Three compounds appear and continue to increase in concentration around this time period: methionine, cysteine, and pyruvic acid. The rise in methionine seems to occur first,



followed by cysteine and pyruvic acid. Many pathways link the metabolism of methionine to cysteine. However, few pathways generate pyruvate from cysteine. Three such pathways are shown in Leninger, A.L., Biochemistry, Worth Publishers, pp.441 (1970). In each of these three pathways, the sulfur group of cysteine is removed and pyruvate is generated thereby linking the rise of each of these compounds with each other as well as to an increase of sulfate within the media.

**[0063]** Sulfate Production within *B. pertussis* culture: The concentration of sulfate was determined on each of the culture samples and compared with *B. pertussis* growth (OD<sub>650</sub>) and time. Figure 5 illustrates the results of these determinations on the same samples used to generate the data in Figure 4. The data demonstrate that at the approximate time when methionine, cysteine, and finally pyruvate increased in concentration, there was also a large increase in the production of sulfate.

**[0064]** Growth of *B. pertussis* and the production of PT in the presence of BaCl<sub>2</sub>: The sulfate ion is a modulator of *B. pertussis* from the virulent phase to the avirulent phase. This modulation is regulated by the proteins BvgS and BvgA which are members of a large family of two component regulatory molecules. Although it has been known for some time that the addition of extraneous sulfate would down regulate the production of several of the virulence factors including PT (Weiss and Hewlett, Ann. Rev. Microbiol. 40:661-686 (1986)), the identification of the compound or compounds that interact with this system remained unknown. In order to determine whether the possible generation of sulfate from cysteine catabolism or another source during the course of *B. pertussis* growth might affect PT production, a way was sought to either inactivate or remove the influence of sulfate from the culture. Barium in the form of BaCl<sub>2</sub> is highly soluble in water (1.8 M at 25°C and 2.8 M at 100°C), whereas BaSO<sub>4</sub> is highly insoluble (10.7 μM at 25°C and 17.7 μM at 100°C). This difference in solubility has often been used to precipitate sulfate out of solution for further measurement. Different concentrations of BaCl<sub>2</sub> were added to the growth media and the growth and production of PT in the culture were compared. These data are shown in Figure 5. The addition of the BaCl<sub>2</sub> at both concentrations enhanced the production of PT per cell in both *B. pertussis* strains as compared to the normal media, albeit more in

strain 9797. It should also be noted that a visible precipitate could be seen accumulating over time in the culture, presumably  $\text{BaSO}_4$ . These data suggest that the negative feedback inhibitor of PT within the culture is sulfate.

**[0065]** Cloning of a Cysteine Sulfinase Desulfinate gene from BP: One of the possible enzymes responsible for the removal of sulfur from cysteine, nifS-like genes, has been cloned and characterized from *E. coli*. Mihara et al., *J. Biol. Chem.* 272:22417-22424 (1997). Using this sequence, a homology was sought in the partial *B. pertussis* genome data base. An open reading frame demonstrating high homology to the nifS genes was found and appropriate PCR primers were synthesized. A PCR product of the appropriate size was generated using *B. pertussis* chromosomal DNA, was cloned into a TA cloning vector pCR<sup>®</sup>II-TOPO and was sequenced using methods known to those of ordinary skill in the art (Figure 7).

**[0066]** Peptide synthesis and purification: A peptide containing the sequence GGGDGSFSGFGDGSFSGFG-OH (SEQ. ID. NO. 5) was synthesized by The Rockefeller University Protein Sequencing Facility using NMP t-butoxycarbonyl chemistry on an ABI 430A peptide synthesizer (Applied Biosystems, Foster City, CA). The peptide was deprotected and removed from the resin by treatment with HF in the presence of anisole (0°C/1h). Preparative purification of the peptide was performed using a C-18 column (2.14 ID x 30 cm)(Dynamax-Rainin, Woburn, MA). The peptide was quantitated by PTC amino acid analysis using a Waters Picotag system (Waters, Milford, MA). The synthesized peptide elute from the C-18 column as a major peak consisting of 95% of the total elution profile. The amino acid composition of the purified peptide was in good agreement with the sequence which was used to synthesize the peptide.

**[0067]** Construction of the peptide affinity column: Superose<sup>®</sup> 6B was activated using the method described by Brandt, et al., *Biochim. Biophys. Acta* 386:196-202 (1975). Briefly, a 50% gel slurry of pre-washed Superose<sup>®</sup> 6B in 0.1 M  $\text{NaH}_2\text{PO}_4$ , pH 8.0, was treated with a solution of 250 mM p-benzoquinone in ethanol to give a final concentration of 20% ethanol and 50 mM p-benzoquinone. The suspension was gently shaken for 1 h at

room temperature. The activated Superose<sup>®</sup> 6B was then extensively washed on a coarse disc sintered glass funnel with 2 volumes each of 20% ethanol, deionized H<sub>2</sub>O, 1 M NaCl, and once again with deionized H<sub>2</sub>O. The activated Superose<sup>®</sup> 6B was aspirated to a compact cake and one volume of a solution containing 2 mg/ml of the peptide in 0.1 M NaHPO<sub>4</sub>, pH 8.0, was added and the mixture rotated end-over-end for 24 h at 4°C. 1.0 M ethanolamine, pH 8.0, was then added and the rotation continued for 1 h at room temperature. The gel matrix was then wash extensively with deionized H<sub>2</sub>O, 1.0 M NaCl in 0.1 M NaHPO<sub>4</sub>, pH 7.0. Aliquots of the initial peptide solution and the supernatant directly after the coupling step were retained and measured by A<sub>280</sub> using a Shimadzu UV Spec 120 (Shimadzu, Columbia, MD) to determine the incorporation of the peptide onto the Superose<sup>®</sup> 6B.

**[0068]** From the foregoing description, one skilled in the art can easily ascertain the essential characteristics of this invention, and without departing from the spirit and scope thereof, can make various changes and modifications of the invention to adapt it to various usages and conditions without undue experimentation. All patents, patent applications and publications cited herein are incorporated by reference in their entirety.